

Mathematical Modelling of the Vacuum Carburizing Process

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The primary goal of simulation is to predict the course of the process and the final properties of the product.

CAs expectations regarding the quality and precision of products continue to grow, further advances in materials engineering are strictly associated with the use of computer assisted computation methods. Computer modelling and simulations facilitate the design of engineering materials and predicting the properties of these materials with significant reduction in time and costs. Thus, the literature contains numerous reports on the subject

(1-11). Computational support is particularly required in vacuum thermochemical processing due to its non-equilibrial nature and transient states in the course of the processes. In this case, the primary goal of simulation is to predict the course of the process and the final properties of the product, thus ensuring the repeatability of process outcomes. The vacuum carburizing model presented in this article is a classic example of a hybrid model, in which:

- · basic phenomena of carburizing lowand medium-carbon steels are described by an analytical mathematical-physical model;
- parameters such as carbon diffusion coefficient D_C and carbon transfer coefficient β were determined by analysis of variance and multiple regression on the basis of experimental data sets;
- phenomena that could not be described by mathematical equations or for which



no mathematical apparatus was available were processed by means of datamining using neural networks;

- phenomena of formation and dissolution of carbon deposits were described by a heuristic model;
- material data regarding steels were collected in a database to eliminate redundant processes and accelerate model operation.

A MATHEMATICAL-PHYSICAL MODEL OF THE VACUUM CARBU-RIZING PROCESS

The mathematical-physical model of the vacuum carburizing process is based on six principles defined by the authors of references [12-14]:

- Carburizing atmosphere in the saturation stage is delivered to the sample surface in a continuous manner.
- Composition of carburizing atmosphere remains constant throughout the process.

- · Carbon atoms are released as a result of catalytic interaction between the atmosphere and the carburized surface.
- Carbon is transported to the material by means of diffusion in accordance with Fick's equations.
- · Carbon diffusion coefficient in austenite depends on the temperature, carbon concentration and the presence of alloy
- Computations are based on a semiinfinite area.

The development of carbon profiles in austenite depends both on the phenomena occurring at the gas-metal interface, and on the diffusion of carbon in austenite. Phenomena occurring at the gasmetal interface that determine the rate in which carbon concentration changes at the surface, including the most important catalytic interactions between the carburizing atmosphere, are reflected in the mathematical model by atomic carbon flux I_C crossing the interface:

$$I_C = -\beta \left[c_A - \left(c(t) \right)_S \right],$$

where: I_C – flux of carbon atoms across the surface of carburized material, c_A – concentration of carbon at equilibrium with the carburizing atmosphere, (c(t))- current concentration of carbon at the material surface, β – coefficient of carbon transport across the gas-metal interface. Carbon transport in austenite has been described on the basis of Fick's diffusion laws. The first law described the flux of the diffusing component:

$$I_C = -D_C \cdot grad[c],$$

where: D_{ϵ} – carbon diffusion coefficient in austenite; the value depends on the temperature, carbon concentration, and the content of alloy additives, grad/c/- gradient of carbon concentration in austenite.

The second law describes the change in carbon concentration as a function of

$$\frac{\partial[c]}{\partial t} = div(grad I_c).$$

In the case of single-directional diffusion the above laws can be expressed in the following manner:

$$I_C = D_C \frac{\partial [c]}{\partial x},$$

The effect of surface phenomena on the profile of carbon diffusion within austenite is taken into consideration by solving Fick's second law at the border condition resulting from the comparison of equations (1) and (4):

$$\frac{\partial[c]}{\partial t} = \frac{\partial}{\partial x} \left(D_C \frac{\partial[c]}{\partial x} \right).$$

Therefore, the problem of determining the profile of carbon concentrations within austenite amounts to solving equation (5) at the border condition (6) and the initial condition (7):

$$-D_{c} \frac{\partial [c]}{\partial x}\Big|_{x=0} = \beta \left[[c]_{A} - (c(t))_{S} \right],$$

COMPUTATIONAL MODEL OF THE VACUUM CARBURIZING PROCESS

Input computational data included process parameters, chemical composition of the material, carbon carrier gas parameters and the geometry of the carburized surface. Coefficients affecting model precision are carbon diffusion coefficient D_C , activity of carbon in austenite a_C , carbon transfer coefficient β and geometry coefficient.

Functions describing the relationship between the carbon diffusion coefficient DC and temperature or time were presented in numerous articles [15-24]. The first studies of the model were based on the carbon diffusion coefficient formula proposed by Goldstein [15]. This relationship soon turned out to be insufficient, and therefore formulas proposed by Leyens [16], Tibbets [17] and the empirical equation proposed by Dybowski in an article dedicated to this issue were successively used in subsequent studies [25]. The last equation provided for the best agreement of the model with actual profiles within the carburizing process temperatures of 860-1010°C.

One of the factors impacting the value of carbon diffusion coefficient D_C is the activity of carbon within austenite in

the presence of alloy additives a_C with the effect of alloy additives on carbon concentration profile being taken into consideration. In addition, the coefficient defining the effect of alloy additives on the activity of carbon within austenite a_C allows for the computation of the maximum solubility of carbon within austenite, C_{gp} , at temperature T for a particular material. Therefore, a_C value was included in the model, making use of the equation provided in [20].

Experimental data set results were used to determine the carbon transfer coefficient β . Multiple regression analysis revealed that the only factor having a statistically significant impact on the value of the carbon transport coefficient is temperature, related to the coefficient by equation (8):

$$\beta = a \cdot e^{b \cdot T}$$

where: β – carbon transfer coefficient, T – temperature, a,b – coefficients.

For better precision of calculations the computational model accounted for the effect of surface geometry on the distribution of carbon within the carburized layer by introducing a correction factor µi based on the data presented in [13]:

$$\mu_i = \left[\tfrac{(r - (i - H)dx)^{3 - H} - (r - (i - 1 + H)dx)^{3 - H}}{(r - (i - 1 - H)dx)^{3 - H} - (r - (i - 2 + H)dx)^{3 - H}} \right]^{RF},$$

where: i – spatial sample of interest in the Crank-Nicolson method, r – curvature radius, H, RF – coefficients listed in Table 1.

COMPUTATION ALGORITHM

The first mathematical algorithm for vacuum carburizing was by Kołodziejczyk in an article dedicated to this topic [13]. Model input parameters include the process, material and surface geometry parameters. The material status is calculated in a matrix consisting of cells representing spots located within the material at every 0.01 mm, in time increments of 0.1 s. Limitations expressed by condition (10) were set onto the time increment and computational step to ensure the convergence and stability of computations. The stability of partial differential computations means that errors are not accumulated as the problem is being solved, while convergence of computations means that an accurate result is obtained in the solution.

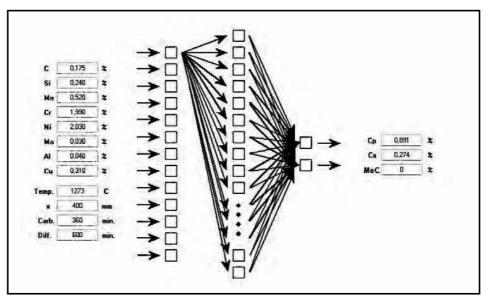


Figure 1: Neuron model for predicting the amount of carbide precipitation following the vacuum carburizing process [29].

$$0 < \frac{{}^{D}c_{gr} \Delta t}{\Delta x^{2}} < \frac{1}{2}$$

where: D_{Cor} – carbon diffusion coefficient calculated for the maximum concentration of carbon within austenite, Δt time increment, Δx — computational step.

Calculations start at the time point t=0and are continued until the process time T_{PROC} reaches the total time resulting from the total of segments (steps) defined in input parameters. The value of the diffusion coefficient during the process depends on several factors simultaneously; thus, the equation describing unidimensional transport of carbon within austenite becomes nonlinear and impossible to solve analytically. Therefore, the issue is solved by numerically using the Crank- Nicolson finite-differences method [26], as well as the Crout factorization and Thomas algorithm.

MODELLING OF FORMATION AND **DISSOLUTION OF CARBIDE PRECIPI-TATIONS**

Carburizing processes carried out above the limit concentration C_{gr} lead to carbide precipitations. These precipitations are gradually dissolved in the hold stage; however, the kinetics of both formation and dissolution follow individual patterns, strongly related to the chemical composition of a particular precipitation. Since the literature lacks comprehensive information on the kinetics of the process, the black box data-mining model was used, as it required no analytical knowledge of the phenomenon of interest. A series

of experimental studies were also conducted in order to better understand this issue; the results are presented in publications [27, 28, 29]. A learning data set was developed on the basis of these results, followed by the development of a neural network reflecting the relationships between process parameters and the properties of the carburized layer, as was also described in detail in the above papers. When choosing the network architecture it was assumed that the network should be extrapolative, i.e. it should possibly correctly predict cases beyond the learning set. This assumption prevailed in the choice of the Multi Layer Perceptron (MLP) networks due to their capabilities in this respect [30].

Carburizing process parameters were defined as network input parameters, including carburizing temperature T_N , segmentation and chemical composition of the material: concentrations of carbon C, silicone Si, manganese Mn, chromium Cr, nickel Ni, aluminum Al, copper Cu; as well as the point of consideration X within the material. The output network signals represented the properties of the carburized layer: surface carbon concentration, C_P ; carbon concentration at distance X from the surface, C_{x} ; as well as the percentage content of carbides at distance X from the surface, MeC.

The search for the best network was started by selecting 2,000 networks with random numbers of hidden neurons and random activation functions. Next, each network was subjected to training to assess its correlations between predicted values and the actual learning sets. The training process made use of back-error propagation methods, including

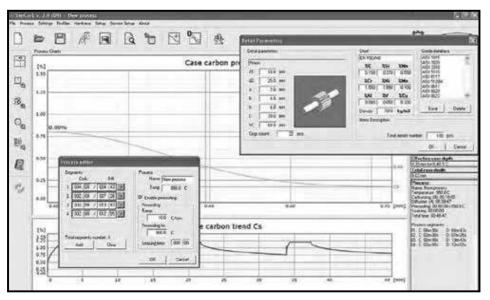


Figure 2: Hybrid vacuum carburizing model (SimVac Plus). Carburizing module.

a momentum factor, the Broyden-Fletcher-Goldfarb-Shanno (BFGS) method and gradient methods to identify the best learning method for each particular network. The sum of squared differences was assumed as the error function. Eventually, the best network was identified as an MLP network with 12 input

neurons, 10 hidden neurons and 3 output neurons, sigmoid hidden neuron activation function, exponential output neuron activation function and the BFGS training method. Network correlation coefficients were 0.982 for the learning data set and 0.952 for the validation data set (scale [0;1]).

CONCLUSIONS

From the industrial standpoint, the quality and usefulness of a technology depends on its ability to ensure required product parameters and repeatability of the process. Therefore, simulation programs based on mathematical models and artificial intelligence methods provide much-required support for the technical features of modern vacuum furnaces, serving as tools for the design and optimization of these furnaces, thus ensuring optimum control of the production process.

The FineCarb® vacuum carburizing technology, followed by gas or oil hardening, is used, e.g. in the production of drive and motion-transferring elements in engineering, in the automotive and aviation industries for the hardening of outer layers of gears, shafts, bearing rings, levers, etc. The presented vacuum carburizing models, along with the gas hardening model, were included in the expert system (Fig. 2) that supports the technology.

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ARGE CAPACITY INTE

Excellent for Surface Combustion (quantity 2) Integral Quench Furnaces Gear Heat 62"W x 62"L x 36"H, max. temp. 1,850°F, Treatment 4,600,000 BTUH, 9,500 gallons, 2 re-circulation fans, four 30 HP Gold Standard agitators, Eclipse burners and recuperative, atmosphere sample system, 2 rear handlers and Allen Bradley Panelview PLC5 with Yokagama instruments.

Surface Combustion (quantity 1) Integral Quench Furnace, 87"W x 87"L x 36"H, max. temp. 1,850°F 4,600,000 BTUH, 12,500 gallons, 2 re-circulation fans, six 30 HP Gold Standard agitators, Eclipse burners and recuperative, atmosphere sample system, 3 rear handlers and Allen Bradley Panelview PLC5 with Yokagama instruments.

Surface Combustion (quantity 1) Wash/Rinse/Dry 87"W x 87"L x 36"H, max. temp. 180°F, 1,500,000 BTUH, oil skimmer, filters and controls.



Atmosphere Temper Furnace 87"W x 87"L x 36"H, max. temp. 1,350°F 1,500,000 BTUH, load/unload by charge car, Eclipse burners and recuperators, 1 combustion blower, 1 common drive, 2 re-circulation fans and Allen Bradley Panelview PLC5 with Yokagama instruments.

Surface Combustion (quantity 1) Double Ended Charge Car 87"W x 87" L, automatic double positioning, extended reach with cable reel and Allen Bradley controls.

Epcon (quantity 1) High Temp Electric Walk-In Oven 72"W x 72"L x 72"H, max. temp. 1,250 °F 2 barn style doors, 1 re-circulation fan, 1 exhaust fan and free standing control panel with controls.



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project is conducted in the framework of a pilot venture "Support research and development on a demonstration scale".

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Geometry	Curvature	H	RF
Flat	_	_	0
Cylindrical	Outer	1	1
	Inner	1	-1
Spherical	Outer	0	1
	Inner	0	-1

Table 1: Values of H and RF for different geometries and curvatures of elements [13].

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