Supplementary Information for

Reaction Kinetics of Green Leaf Volatiles with Sulfate, Hydroxyl and Nitrate Radicals in Tropospheric Aqueous-Phase

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1. PROPERTIES OF GLVs STUDIED

GLV	Molecular formula	The Henry's Law Constant for water	Vapor pressure	Water solubility
		mol L ⁻¹ atm ⁻¹	atm	mg L ⁻¹
1-penten-3-ol	C ₅ H ₁₀ O	101.22	1.20×10 ⁻²	4.53×10^{4}
(Z)-2-hexen-1-ol	$C_6H_{12}O$	133.26	1.19×10 ⁻³	1.60×10^4
(E)-2-hexen-1-al	C ₆ H ₁₀ O	10.12	6.21×10 ⁻³	5.26×10 ³

Table S1. Physical properties of selected GLVs at 298 K estimated with EPI suite¹

2. LFP-LLPA EXPERIMENTAL SETUP

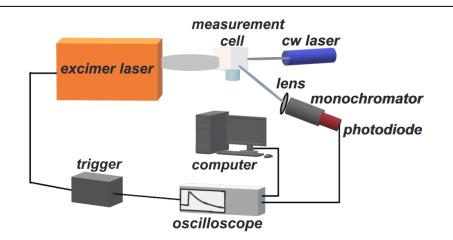


Figure S1. The Laser Flash Photolysis-Laser Long Path Absorption (LFP-LLPA) setup used for the kinetic investigations.

• **3. UV SPECTROSCOPY OF GLV**

The molar absorption coefficients of GLVs were determined from absorption spectra measured with a Lambda 900 UV/VIS/NIR spectrometer (Perkin Elmer Instruments). The UV spectra were recorded over the wavelength range of 200 - 400 nm and for the concentrations ranging from 500 - 31.25 mM (PENTOL); 100 - 6.25 mM (HEXOL); 30 - 1.875 mM (HEXAL). Molar absorption coefficients were determined at 248, 308, and 351 nm using the average of experimental molar extinction coefficients at each concentration point. For (E)-2-hexen-1-al, the absorbance could be

recorded only at wavelengths longer than 245 nm. The uncertainties of the coefficients were equal Vto the standard deviations (shown as yellow ranges).

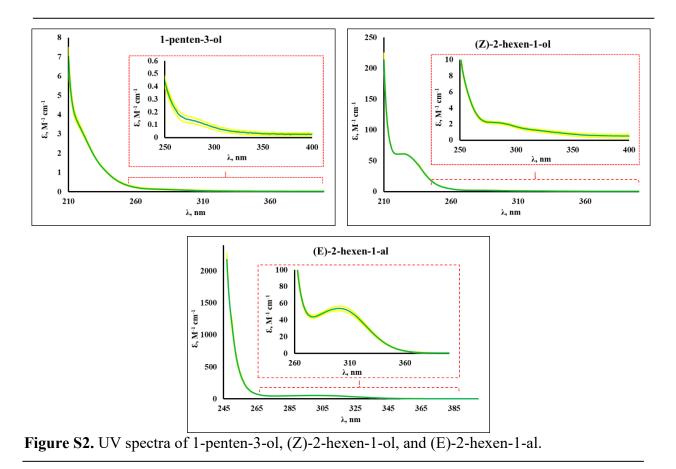


Table S2 shows the molar absorption coefficients' values at three wavelengths, which were used to correct the internal filter effects (explained in the main text) due to GLV reactants in experiments with 'OH radicals (Table S3).

	Table S2. Selected numerical values of the molar absorption coefficients of the examined GLVs used to calculate the filter effects in Table S3.						
Wavelength		ε					
nm		$L \text{ mol}^{-1} \text{ cm}^{-1}$					
	1-penten-3-ol	(Z)-2-hexen-1-ol	(E)-2-hexen-1-al				
248	0.51 ± 0.03	13.3 ± 0.4	1722 ± 13				
308	0.06 ± 0.02	1.4 ± 0.2	51.8 ± 2.8				
351	0.03 ± 0.01	0.7 ± 0.2	6.4 ± 0.3				

d

Experiment	[GLV]	[OH] ₀ change, %				
	10 ⁻⁴ L mol ⁻¹	1-penten-3-ol	(Z)-2-hexen-1-ol	(E)-2-hexen-1-al		
		at 248 nm	at 248 nm	at 308 nm		
Ι	0.5	0.01	0.23	0.87		
II	1.0	0.02	0.45	1.74		
III	1.5	0.03	0.68	2.59		
IV	2.0	0.03	0.90	3.44		

Table S3. Change in the initial 'OH concentrations due to a GLV as an internal filter of the UV light.

• 4. EXPERIMENTAL DETAILS

Radical GLV		Radical precursor	Excimer laser	Continuous- wave laser	Total path length
			λ, nm	λ, nm	cm
SO4	1-penten-3-ol		248	407	32
	(Z)-2-hexen-1-ol	$Na_2S_2O_8$	248	407	
	(E)-2-hexen-1-al		308	473	
•ОН	1-penten-3-ol		248	407	32
	(Z)-2-hexen-1-ol	H_2O_2	248	407	
	(E)-2-hexen-1-al		308	473	
NO3 [•]	1-penten-3-ol				
	(Z)-2-hexen-1-ol	NaNO ₃	351	635	128
	(E)-2-hexen-1-al				

 Table S4. Photolysis setup for different radical generation and measurement

		SO 4	'OH		I NO3	
GLV	[GLV]	Na2S2O8	H2O2	KSCN	NaNO3	Na2S2O8
1-penten-3-ol	0.005 - 0.2	0.5	0.2	0.02	100	30
(Z)-2-hexen-1-ol	0.01 - 0.2	0.5	0.2	0.02	100	30
(E)-2-hexen-1-al	0.0025 - 0.2	5.0	10	0.20	100	30

Table S5: Initial concentrations of reactants (mM) in the kinetic experiments with GLVs.

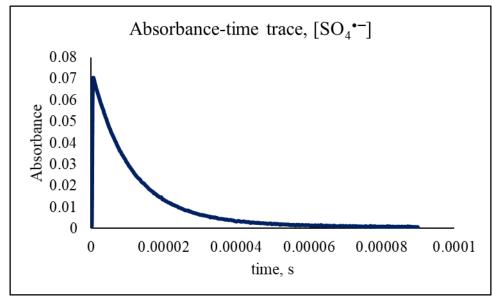


Figure S3. Typical absorbance-time traces observed following a laser flash photolysis. Here shown as an example from $Na_2S_2O_8$ (0.5 mM) and 1-penten-3-ol (0.1 mM) mixture in the water at 298 K showing the rapid decay of the sulfate radical-ion.

5. ACTIVATION PARAMETERS

Calculation of activation parameters is described in detail elsewhere. ²⁻⁴ The activation parameters were calculated using the equations (S1-S4).

Arrhenius equation:
$$k(T) = A \exp \frac{-E_A}{RT}$$
 (S1)

Enthalpy of activation:	$\Delta H^{\ddagger} = E_A - RT$	(S2)
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Entropy of activation:	$\Delta S^{\ddagger} = R \left[\ln A - \ln \frac{k_B T}{h} - 1 \right]$	(S3)
Gibb's free energy of activation:	$\Delta G^{\ddagger} = \Delta H^{\ddagger} - T \Delta S^{\ddagger}$	(S4)

where: Boltzmann constant $k_B = 1.38 \times 10^{23} JK^{-1}$, Planck constant $h = 6.626 \times 10^{-34} Js$.

6. DIFFUSIONAL LIMITATION OF CHEMICAL REACTIONS

An experimentally observed second-order rate constant that is limited by the diffusion of reactants, k_{obs} , can be split into the true rate constant k_{reac} and the diffusion rate constant k_{diff} using a simple resistance-in-series approach:

$$k_{obs}^{-1} = k_{reac}^{-1} + k_{diff}^{-1}$$
(S5)

The diffusion rate constant is calculated using the Smoluchowski Equation (S11):5

$$k_{diff} = 4 \times 10^3 \pi N_A (D_A + D_B) (r_A + r_B)$$
(S6)

where: N_A is the Avogadro number, D_A and D_B (m² s⁻¹) are the diffusion coefficients of reactants, r_A and r_B (m) are reaction radii of the reactants.

The diffusion coefficients are calculated using the Stoke-Einstein relationship modified by Wilke and Chang: ⁶

$$D = 7.4 \times 10^{-12} \frac{(XM)^{0.5}T}{V_m^{0.6}\eta}$$
(S7)

where: X is the association parameter of a solvent (2.26 for water), M is the molar mass of a diffusing compound, cm³ mol⁻¹, T is the absolute temperature in K, V_m is the molar volume of a diffusing compound⁷, η is the dynamic viscosity of the solvent, mPa or 0.01 g cm⁻¹ s⁻¹ (0.8891 mPa for water at 298 K). Molar volumes for reactants in the present work are given in Table S8.

The reaction radii of the reacting compounds were calculated using the procedure of Kojima and Bard (1975)⁸

$$r = \sqrt[3]{\frac{3 \times V_m}{4 \times \pi \times N_A}} \tag{S8}$$

The radical radii were adopted from Buxton et al., 1988 (*OH),⁹ and Nightingale et al., 1959 (SO₄ •- & NO₃ •).¹⁰ The radical molar volumes were adopted from Schöne et al. 2014,³ whereas the molar volumes of the organic compounds were calculated using Tyn and Claus method (1975) given in equation (S9)¹¹ and critical volume described by Joback and Reid, 1987 (equation S10)⁷ at the boiling point. The final molar volume at measurement temperatures were obtained using the ideal gas approach (V_m/T= constant).

$$V_m = 0.285 \times V_c^{1.048} \tag{S9}$$

$$V_C = 17.5 + \Sigma \Delta V \tag{S10}$$

Molecule	V _m r		D (at 298 K)	
	cm ³ mol ⁻¹	nm	10 ⁻⁹ m ² s ⁻¹	
SO4	61.5 ^a	0.29 ^a	1.30	
.OH	26.9 ^a	0.22 ^a	2.20	
NO ₃ ·	46.4 ^a	0.264 ^a	1.54	
1-penten-3-ol	89.4 ^b	0.329	1.06	
(Z)-2-hexen-1-ol	95.2 ^b	0.335	1.03	
(E)-2-hexen-1-al	99.2 ^b	0.340	1.00	

Table SG. D. +: f +:. looul

^a Schöne et al.³; ^b Estimated using Joback method.⁷

Table S7. Comparison of experimentally observed and diffusion-corrected rate constants for reactions of GLVs with SO₄⁻, and rate constants for the diffusion of reactants (k_{obs} , k_{reac} , and k_{diff} , respectively, 10⁸ L mol⁻¹ s⁻¹).

GLV + SO4		278 K	288 K	298 K	308 K	318 K
	<i>k</i> _{obs}	8.2 ± 0.7	9.4 ± 0.7	9.4 ± 1.0	10.5 ± 2.1	11.0 ± 2.4
PENTOL	k _{reac}	9.0 ± 0.8	10.4 ± 0.8	10.2 ± 1.1	11.5 ± 2.3	12.1 ± 2.7
	k_{diff}	88.2	98.8	111	124	126
	$\% k_{diff}$	9	10	9	9	9
HEXOL	kobs	17.1 ± 2.0	22.0 ± 3.3	25.3 ± 3	28.1 ± 6.5	28.7 ± 6.3
	k _{reac}	21.2 ± 2.5	28.4 ± 4.2	32.9 ± 3.9	36.4 ± 8.5	37.3 ± 8.2
	k_{diff}	88.1	98.4	110	123	125
	$\% k_{diff}$	19	22	23	23	23
	<i>k</i> _{obs}	4.2 ± 0.2	4.5 ± 0.1	4.8 ± 0.2	5.3 ± 0.3	5.1 ± 0.5
HEXAL	kreact	4.4 ± 0.2	4.7 ± 0.1	5.0 ± 0.2	5.6 ± 0.3	5.4 ± 0.5
	k_{diff}	88.1	98.3	110	123	124
	% k _{diff}	5	5	4	4	4

GLV + 'OH		278 K	288 K	298 K	308 K	318 K
PENTOL	<i>k</i> _{obs}	4.01 ± 0.04	5.1 ± 0.2	6.3 ± 0.1	6.5 ± 0.3	8.5 ± 1.0
	<i>k</i> _{reac}	6.2 ± 0.1	8.7 ± 0.3	11.8 ± 0.3	11.5 ± 0.6	19.8 ± 2.4
	k_{diff}	11.5	12.5	13.6	14.8	14.9
	$\% k_{diff}$	35	41	46	44	57
	<i>k</i> _{obs}	4.49 ± 0.04	5.4 ± 0.2	6.7 ± 0.3	6.3 ± 0.3	7.8 ± 0.4
	<i>k</i> _{reac}	7.4 ± 0.1	9.5 ± 0.3	13.1 ± 0.6	11.0 ± 0.4	16.4 ± 0.8
HEXOL	k_{diff}	11.5	12.5	13.6	14.8	14.9
	% k _{diff}	39	43	49	43	52
	kobs	3.5 ± 0.1	4.6 ± 0.1	4.8 ± 0.3	6.0 ± 0.3	6.6 ± 0.4
HEXAL	k _{reac}	4.9 ± 0.2	7.4 ± 0.2	7.4 ± 0.5	10.1 ± 0.5	12.0 ± 0.7
	k_{diff}	11.6	12.5	13.6	14.7	14.9
	$\% k_{diff}$	30	37	35	41	45

Table S8. Comparison of experimentally observed and diffusion-corrected rate constants for reactions of GLVs with 'OH, and rate constants for the diffusion of reactants (k_{obs} , k_{reac} , and k_{diff} , respectively, 10⁹ L mol⁻¹ s⁻¹).

GLV + NO3 [•]		278 K	288 K	298 K	308 K	318 K	
	<i>k</i> _{obs}	8.8 ± 1.6	10.5 ± 2.3	15.0 ± 1.5	19.8 ± 4.2	21 ± 9	
PENTOL	k _{reac}	8.9 ± 1.6	10.6 ± 2.3	15.2 ± 1.5	20.1 ± 4.3	20.6 ± 9.2	
PENIOL	k_{diff}	950	1053	1169	1297	1313	
	% k _{diff}	1	1	1	2	2	
	<i>k</i> _{obs}	64.3 ± 14.8	79.1 ± 24.3	83.7 ± 22.8	97.7 ± 39.3	83 ± 19*	
HEXOL	kreac	69 ± 16	85.5 ± 26.2	90.2 ± 24.6	105.7 ± 42.5	-	
HEAOL	<i>k</i> _{diff}	951	1051	1165	1290	-	
	$\% k_{diff}$	7	8	7	8	-	
	<i>k</i> _{obs}	2.0 ± 0.6	2.1 ± 0.2	3.0 ± 0.7	3.7 ± 0.1	5.0 ± 0.8	
HEXAL	k _{reac}	2.0 ± 0.6	2.2 ± 0.2	3.0 ± 0.7	3.7 ± 0.1	5.0 ± 0.8	
пелаl	k_{diff}	952	1050	1160	1290	1300	
	$\% k_{diff}$	0.2	0.2	0.3	0.3	0.4	
* at T = 293 K							

Table S9. Comparison of experimentally observed and diffusion-corrected rate constants for reactions of GLVs with NO₃, and rate constants for the diffusion of reactants (k_{obs} , k_{reac} , and k_{diff} , respectively, 10⁷ L mol⁻¹ s⁻¹).

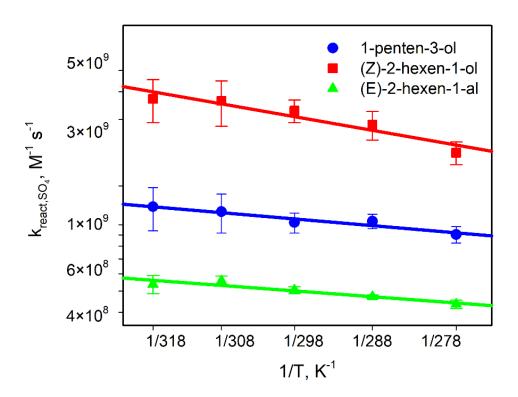


Figure S4a. Arrhenius plots of the rate constants corrected for diffusional limitations, k_{reac} for the reaction of GLVs with SO₄⁻⁻ (see Table S7 for the numerical values of the constants).

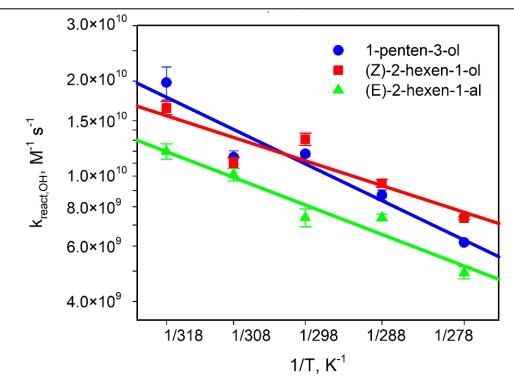


Figure S4b. Arrhenius plots of the rate constants corrected for diffusional limitations, k_{reac} for the reaction of GLVs with 'OH (see Table S8 for the numerical values of the constants).

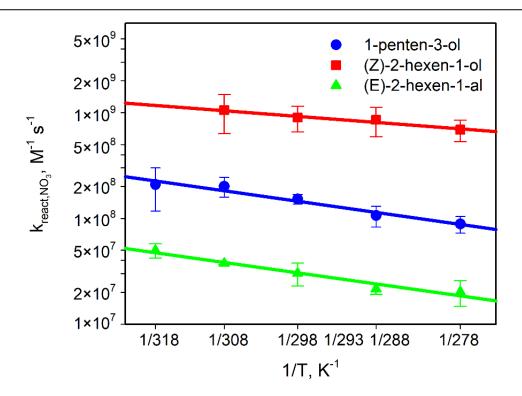


Figure S4c. Arrhenius plots of the rate constants corrected for diffusional limitations, k_{reac} for the reaction of GLVs with NO₃[•] (see Table S9 for the numerical values of the constants).

Table S10. The diffusion-corrected activation parameters for the reactions of GLVs with SO₄[•], [•]OH and NO₃[•] radicals.

Reactants		E_A	A	ΔH^{\ddagger}	- ΔS^{\ddagger}	$\Delta {m G}^{\ddagger}$
		kJ mol ⁻¹	L mol ⁻¹ s ⁻¹	kJ mol ⁻¹	J mol ⁻¹ K ⁻¹	kJ mol ⁻¹
	PENTOL	5 ± 1	$(8.0 \pm 0.1) \times 10^9$	3 ± 1	64 ± 1	22 ± 5
SO 4	HEXOL	10 ± 2	$(19 \pm 1) \times 10^{10}$	8 ± 2	37 ± 1	19 ± 5
	HEXAL	4 ± 1	$(2.9 \pm 0.1) \times 10^9$	2 ± 1	72 ± 2	23 ± 6
	PENTOL	19 ± 3	$(2.5 \pm 0.1) \times 10^{13}$	17 ± 4	-3.2 ± 0.2	16 ± 4
•OH	HEXOL	13 ± 3	$(2.1 \pm 0.1) \times 10^{12}$	11 ± 3	17 ± 1	16 ± 6
	HEXAL	15 ± 2	$(3.9 \pm 0.2) \times 10^{12}$	13 ± 2	12 ± 1	17 ± 4
	PENTOL	17 ± 2	$(1.6 \pm 0.1) \times 10^{11}$	15 ± 2	39 ± 2	26 ± 5
NO3 [•]	HEXOL	9 ± 1	$(4 \pm 1) \times 10^{10}$	7 ± 1	50 ± 1	22 ± 4
	HEXAL	17 ± 2	$(3.2 \pm 0.1) \times 10^{10}$	15 ± 2	52 ± 2	30 ± 6

• 7. ATMOSPHERIC SIGNIFICANCE

Atmospheric lifetimes, the background. Washing a GLV from the atmosphere's gas phase by combined gas-phase and aqueous-phase reactions with a radical *X* is approximately described by Equation (S11).

$$\frac{d[GLV]_g}{dt} = -\left(k_g[X]_g[GLV]_g + k_{aq}[X]_{aq}[GLV]_{aq}\omega\right)$$
(S11)

where: k_g and k_{aq} , L mol⁻¹ s⁻¹ are the second-order rate constants for reactions of the GLV with X in the gas and aqueous phase, respectively; ω , m³ m⁻³ is the liquid water contents of the atmospheric system; []_g and []_{aq}, M are the concentrations in the gas- and aqueous phases, respectively. We assume that the gas- and aqueous forms of the reactants are bound by Henry's Law equilibria (S12) and (S13).

$$[GLV]_{aq} = H_{d,GLV}[GLV]_g \tag{S12}$$

$$[X]_g = \frac{[X]_{aq}}{H_{d,X}}$$
(S13)

with dimensionless Henry's constants H_d defined by Equations (S14).

$$H_d = HRT, \text{ if } H \text{ is in mol } L^{-1} \text{atm}^{-1}$$
(S14a)

$$H_d = HRT\rho, \text{ if } H \text{ is in mol } \text{kg}^{-1} \text{atm}^{-1}$$
(S14b)

where: *R*, atm L mol⁻¹ K⁻¹ is the gas constant; ρ kg L⁻¹ is the density of solution. Equations (S11) - (S13) are combined and rearranged to Equation (S15).

$$\frac{d[GLV]_g}{[GLV]_g} = -\left(\frac{k_g}{H_{d,X}} + k_{aq}H_{d,GLV}\omega\right)[X]_{aq}dt$$
(S15)

Equation (S18) is integrated within the borders (t, $[GLV]_0$) and (t, [GLV]) to give (S16).

$$ln\left(\frac{[GLV]_g}{[GLV]_{g,0}}\right) = -\left(\frac{k_g}{H_{d,X}} + k_{aq}H_{d,GLV}\omega\right)[X]_{aq}t$$
(S16a)

or
$$\frac{[GLV]_g}{[GLV]_{g,0}} = exp\left(-\left(\frac{k_g}{H_{d,X}} + k_{aq}H_{d,GLV}\omega\right)[X]_{aq}t\right)$$
(S16b)

Now, we define the lifetime of a GLV, t_{life} , as the time in which the concentration of this GLV decreases to $[GLV]_0/e$. We insert this value to Equation (S16b) to get (S17).

$$\frac{1}{e} = exp\left(-\left(\frac{k_g}{H_{d,X}} + k_{aq}H_{d,GLV}\omega\right)[X]_{aq}t_{life}\right)$$
(S17a)

S14

or
$$t_{life} = \frac{1}{\left(\frac{k_g}{H_{d,X}} + k_{aq}H_{d,GLV}\omega\right)[X]_{aq}}$$
 (S17b)

Per analogiam, the lifetime of a GLV consumed by a reaction with a radical *X*, which exists only in the aqueous-phase and does not partition to the gas phase, is given by Equation (S18).

$$t_{life,aq} = \frac{1}{k_{aq}H_{d,GLV}\omega[X]_{aq}}$$
(S18)

When a GLV disappears solely by the reaction with a radical *X*, which does not partition to the aqueous phase, its lifetime is given by Equation (S19).

$$t_{life,g} = \frac{H_{d,X}}{k_g[X]_{aq}} \tag{S19}$$

If a GLV is removed from the atmosphere by the combined gas-phase and aqueous-phase reactions, and one wants to separate those processes virtually, equations (S18) and (S19) help. Table S11 contains the constants required to apply the above equations to GLVs studied in this work.

GLV/radical	Gas-phase rate constants		Gas-phase ra	H_d		
	cm ³ mo	lecule ⁻¹ s ⁻¹	L mo	L mol ⁻¹ s ⁻¹		
	koн	k _{NO3}	k _{OH}	k _{NO3}		
DENTEOL	6.7×10 ^{-11, 12}	13.9×10 ^{-15, 14}	3.7×10 ¹⁰	8.4×10 ⁶	2.5×10 ³	
PENTOL	5.7×10 ^{-11, 13}					
HEXOL	6.2×10 ^{-11, 1}	1.6×10 ^{-13, 15}	3.7×10 ¹¹	9.4×10 ⁷	3.3×10 ³	
HEXAL	4.4×10 ^{-11, 16}	1.2×10 ^{-14, 16}	2.6×10 ¹¹	6.1×10 ⁶	2.5×10 ²	
ЮН					6.1×10 ²	
NO ₃ ·					14.7	

Table S11. Gas-phase rate constants of GLVs with atmospheric radicals at 298 K and dimensionless Henry's constant of GLVs and radicals.

*originally, the gas phase rate constants were reported in cm^3 molecule⁻¹ s⁻¹, and were converted to L mol⁻¹ s⁻¹ for the convenience of present calculations.

Radical	low		high		extremely high		
	mol L ⁻¹		mol L ⁻¹		mol L ⁻¹		
ЮН	urban clouds	3.5×10 ⁻¹⁵	maritime aerosol	1.0×10 ⁻¹³	maritime clouds	2.0×10 ⁻¹²	
	remote clouds	2.2×10 ⁻¹⁴	urban aerosol	4.4×10 ⁻¹³	remote aerosol	3.0×10 ⁻¹²	
NO ₃ .	remote clouds	5.1×10 ⁻¹⁵	remote aerosol	3.5×10 ⁻¹³			
	maritime aerosol	1.9×10 ⁻¹⁵	urban clouds	1.4×10 ⁻¹³			
	maritime clouds	6.9×10 ⁻¹⁵	urban aerosol	8.6×10 ⁻¹⁴			
SO4	maritime clouds	2.3×10 ⁻¹⁵	remote clouds	2.4×10 ⁻¹⁴	remote aerosol	3.6×10 ⁻¹²	
	urban aerosol	9.3×10 ⁻¹⁵	maritime aerosol	1.2×10 ⁻¹⁴			
			urban clouds	1.1×10 ⁻¹⁴			

Table S12. Aqueous-phase concentrations of 'OH, NO₃' and SO₄'⁻ radicals in various atmospheric systems from CAPRAM modeling.¹⁷

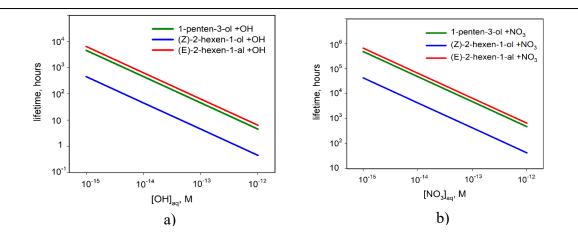


Figure S5. Apparent lifetimes of GLVs due only to the gas-phase reactions with (a) 'OH and (b) NO₃'.

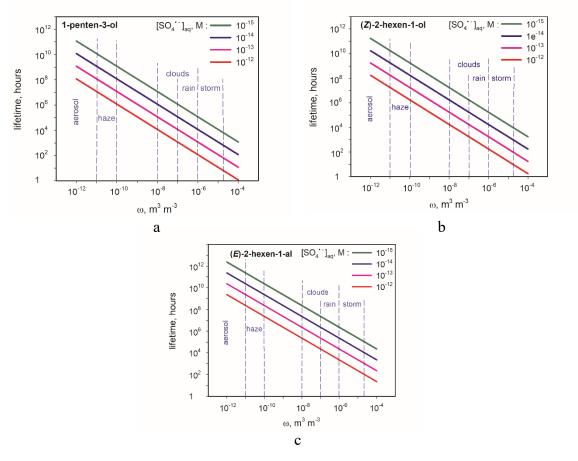


Figure S6. Atmospheric lifetimes of GLVs due to the aqueous-phase reactions with SO_4^- at various liquid water contents (ω): (a) PENTOL, (b) HEXOL, (c) HEXAL.

GLV removal rates – Gas-phase vs. aqueous-phase reactions. Equation (S20) compares a GLV removal from the atmosphere by a gas-phase reaction with a radical X with that GLV removal by the aqueous-phase reaction with SO₄⁻.

$$\frac{r_{X,g}}{r_{SO_4,aq}\omega} = \frac{k_{X,g}}{k_{SO_4,aq}H_{d,X}H_{d,GLV}\omega} \cdot \frac{[X]_{aq}}{[SO_4^-]_{aq}}$$
(S20)

Figure (S7) shows the ratios calculated with Equation (S20) for various ω and proportions of radicals. Aqueous-phase reaction of SO₄⁻⁻ with PENTOL dominates over the gas-phase reaction with 'OH in systems with high liquid water contents provided that SO₄⁻⁻ is in excess: ['OH]/[SO₄⁻⁻] < 0.2, and dominates in clouds and rains over the gas-phase reaction with NO₃⁻ if: [NO₃⁻]/[SO₄⁻⁻] < 20. The conditions which secure a similar dominance of GLV reactions with SO₄⁻⁻ for HEXOL are: ['OH]/[SO₄⁻⁻] < 0.01 and [NO₃⁻]/[SO₄⁻⁻] < 10; and for HEXAL – ['OH]/ [SO₄⁻⁻] < 0.01 and [NO₃⁻]/[SO₄⁻⁻] < 1.

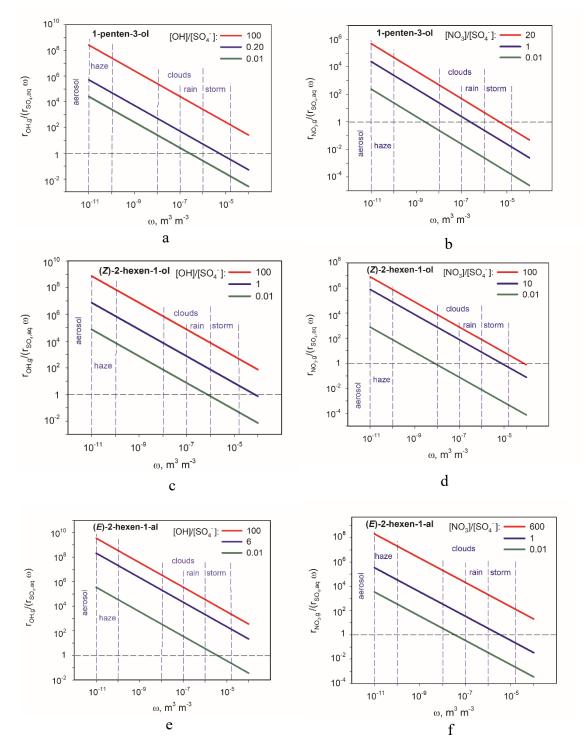


Figure S7. Influence of the liquid water contents (ω) and radical ratios on the relative rates of GLV removal from the atmosphere by gas-phase reactions with 'OH (a,c,e) or NO₃' (b,d,f) and by the aqueous-phase reactions with SO₄'- defined by Equation (S20).

Equation (19) in the main text compares GLV removal from the atmosphere by gas- and aqueous-phase reactions with X ('OH and NO₃') and by the aqueous-phase reactions with SO₄^{•-}. Figure S8 shows the ratios calculated with that equation.

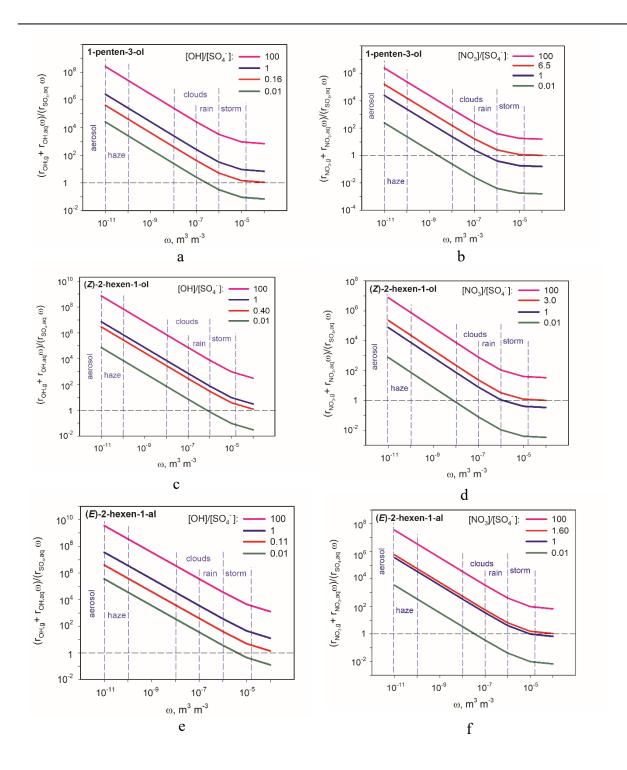
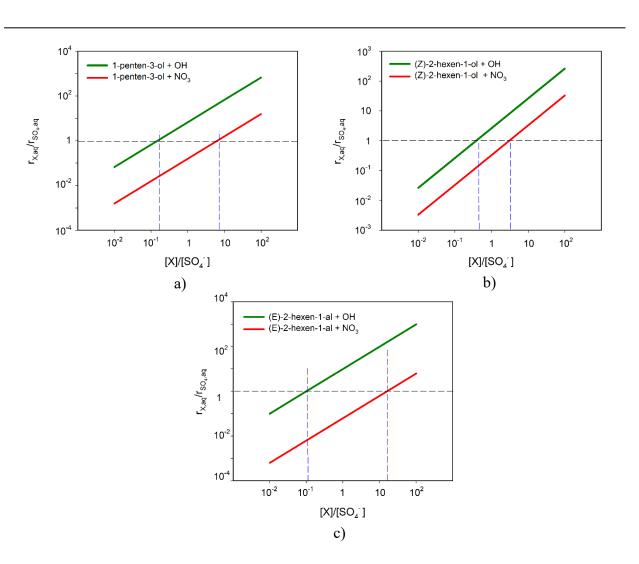


Figure S8. Influence of the liquid water contents (ω) and radical ratios on the relative rates of GLV removal from the atmosphere by combined gas-phase and aqueous-phase reactions with 'OH (a,c,e) or NO₃' (b,d,f) and by the aqueous-phase reactions with SO₄'.

GLV removal rates – **aqueous-phase reactions.** Equation (S21) compares a GLV removal from the atmosphere by an aqueous-phase reaction with a radical X with that GLV removal by the aqueous-phase reaction with SO₄.



$$\frac{r_{X,aq}}{r_{SO_4,aq}} = \frac{k_{X,aq}}{k_{SO_4,aq}} \cdot \frac{[X]_{aq}}{[SO_4^-]_{aq}}$$
(S21)

Figure S9. Influence of the radical ratio on the relative rates of GLVs removal from the atmosphere by the aqueous-phase reaction with 'OH or NO₃' radicals and by the aqueous-phase reactions with SO₄' radical-anions: (a) PENTOL, (b) HEXOL, (c) HEXAL (Equation S21).

Figure S9 shows the ratios calculated with equation (S21) for various ratios of the radicals. Aqueous-phase reaction of PENTOL with SO₄⁻⁻ dominates over the aqueous-phase reaction with 'OH radicals provided ['OH]/[SO₄⁻⁻] < 0.15, and dominates over the aqueous-phase reaction with

NO₃[•] provided [NO₃[•]]/[SO₄^{•-}] < 9. Similarly, the conditions at which the reaction of SO₄^{•-} radicalanions with HEXOL dominate are: [•OH]/[SO₄^{•-}] < 0.8 and [NO₃[•]]/[SO₄^{•-}] < 6. For HEXAL the condition is: [•OH]/[SO₄^{•-}] < 0.11 and [NO₃[•]]/[SO₄^{•-}] < 1.6.

GLV partitioning between gas and aqueous phases. If the gas-aqueous partitioning of a GLV is governed by the Henry's Law equilibrium, the partitioning of that GLV between gas and aqueous phases is given by equation S22 and Fig. S10:

$$\frac{[GLV]_g}{[GLV']_{aq}} = \frac{[GLV]_g}{[GLV]_{aq}\omega} = \frac{1}{H_d\omega}$$
(S22)

where: [GLV']aq is the GLV concentration in the aqueous phase per volume of the gas phase, while other quantities were defined in previous sub-sections.

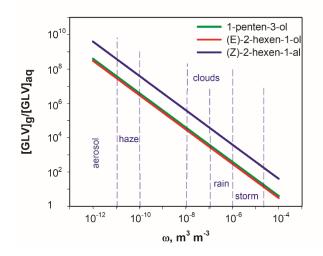


Figure S10. Gas-aqueous partitioning of GLV in various atmospheric systems.

Similar evaluation shows that the OH and NO_3 radicals reside predominantly in the gas phase while the SO_4 radicals – exclusively in the aqueous phase.

8. BIAS OF THE EXPERIMENTAL RATE CONSTANTS FOR NO₃ REACTIONS WITH GLV.

Model_1

Model_1 was built to evaluate the bias of experimentally determined rate constants for reactions of GLVs with NO₃[•] radicals. The bias resulted from the additional consumption of NO₃[•] radicals in several reactions neglected in the experimental method (it assumed the radicals were consumed by a GLV only). The possible "competing" reactants included ⁻OH, H₂O, HO₂[•], and S₂O₈²⁻ and

peroxy radicals derived from alkoxy radicals produced in reaction of SO₄⁻⁻ radicals with a GLV. Table S13 shows all reactions included in Model_1 along with rate constants and Arrhenius parameters. Most of the kinetic parameters were taken from the literature. The rate constants for reactions (13), (15), (24), and (25) in Table S13 were estimated in this work using the COmplex PAthway SImulator (COPASI) software (see the section below Table S13). The temperature-dependent rate constants used within the COPASI model for reaction 32 (Table S13) were determined experimentally within this study.

No	Reaction	k (298 K)	References	A	E_A	Ref., <i>E</i> _A (calc./estd.)	
				L mol ⁻¹ s ⁻¹	kJ mol ⁻¹		
1	$H_2O \rightleftharpoons H^+ + OH^-$	$\rightarrow 0.0014 \text{ s}^{-1}$	18	$\rightarrow 9.9 \times 10^9$	73	19	
		$\leftarrow 1.4 \times 10^{11} \mathrm{L} \mathrm{mol}^{-1} \mathrm{s}^{-1}$		← 5.5×10 ¹³	15		
2	$H_2SO_4 \rightleftharpoons H^+ + HSO_4^-$	$\rightarrow 5.0 \times 10^{13} \text{s}^{-1}$	20	-	-	-	
		$\leftarrow 5.0 \times 10^{10} \text{ L mol}^{-1}\text{s}^{-1}$					
3	$\mathrm{HSO}_{4}^{-} \rightleftharpoons \mathrm{H}^{+} + \mathrm{SO}_{4}^{2-}$	$\rightarrow 1.0 \times 10^9 \mathrm{s}^{-1}$	20	-	-	-	
		$\leftarrow 1.0 \times 10^{11} \text{ L mol}^{-1}\text{s}^{-1}$					
4	$HNO_3 \rightleftharpoons H^+ + NO_3^-$	$\rightarrow 1.1 \times 10^{12} \mathrm{s}^{-1}$	20	-	-	-	
		$\leftarrow 5.0 \times 10^{10} \text{ L mol}^{-1} \text{s}^{-1}$					
5	$HO_2 \rightleftharpoons H^+ + O_2^-$	$\rightarrow 1.4 \times 10^6 \mathrm{s}^{-1}$	18	$\rightarrow 1.3 \times 10^9$	17	19	
		$\leftarrow 5.0 \times 10^{10} \text{ L mol}^{-1} \text{s}^{-1}$		← 5.1×10 ¹²	12		
6	$OH + OH \rightarrow H_2O_2$	3.6×10 ⁹ L mol ⁻¹ s ⁻¹	21	7.9×10 ¹⁰	8	19	
7	$^{\circ}OH + H_2O_2 \rightarrow H_2O + HO_2^{\circ}$	2.7×10 ⁷ L mol ⁻¹ s ⁻¹	293 K, 22	5.3×10 ⁸	7	22	
8	$^{\circ}\text{OH} + \text{HO}_{2}^{\circ} \rightarrow \text{H}_{2}\text{O} + \text{O}_{2}^{\circ}$	6.0×10 ⁹ L mol ⁻¹ s ⁻¹	21	8.2×10 ¹¹	12	21	
9	$^{\bullet}\text{OH} + \text{O}_2^{\bullet} \rightarrow \text{OH}^- + \text{O}_2$	1.1×10 ¹⁰ L mol ⁻¹ s ⁻¹	22	2.9×10 ¹⁰	2	19	
10	$^{\circ}\text{OH} + \text{HSO}_{4}^{-} \rightarrow \text{SO}_{4}^{-} + \text{H}_{2}\text{O}$	3.5×10 ⁵ L mol ⁻¹ s ⁻¹	23	2.0×10 ⁷	10	c	
11	$SO_4^{-} + H_2O \rightarrow OH + HSO_4^{-}$	7.9 L mol ⁻¹ s ⁻¹	23	4.1×10 ³	16	24	
12	$SO_4^{\bullet} + HNO_3 \rightarrow NO_3^{\bullet} + HSO_4^{\bullet}$	5.5×10 ⁵ L mol ⁻¹ s ⁻¹	25	1.0×10 ⁸	13	26	
13	$SO_4^{-} + NO_3^{-} \rightarrow NO_3^{+} + SO_4^{2-}$	9.0×10 ⁴ L mol ⁻¹ s ⁻¹	27				
		9.2×10 ⁴ L mol ⁻¹ s ⁻¹	*	4.1×10 ⁸	21	*Table S14	
14	$SO_4^{\bullet} + HO_2^{\bullet} \rightarrow HSO_4^{\bullet} + O_2$	3.5×10 ⁹ L mol ⁻¹ s ⁻¹	28	5.2×10 ⁹	1	26	

Table S13. Model_1 – reactions with temperature-dependent rate constant
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15	$SO_4^- + S_2O_8^2 \longrightarrow S_2O_8^- + SO_4^2$	1.0×10 ⁴ L mol ⁻¹ s ⁻¹	24			
		1.4×10 ⁴ L mol ⁻¹ s ⁻¹	*	2.2×10 ⁶	-60	*Table S15
16	$SO_4^+ + OH \rightarrow HSO_5^-$	1.0×10 ¹⁰ L mol ⁻¹ s ⁻¹	29	1.5×10 ¹⁰	1	26
17	$SO_4^{\bullet} + SO_4^{\bullet} \rightarrow S_2O_8^{2\bullet}$	2.0×10 ⁸ L mol ⁻¹ s ⁻¹	24	4.0×10 ⁸	2	24
18	$SO_4^{\bullet} + HSO_5^{\bullet} \longrightarrow HSO_4^{\bullet} + SO_5^{\bullet}$	1.0×10 ⁵ L mol ⁻¹ s ⁻¹	30	1.9×10 ⁷	13	26
19	$SO_4^{\bullet} + OH^{-} \rightarrow SO_4^{2-} + {}^{\bullet}OH$	1.4×107 L mol ⁻¹ s ⁻¹	31	1.8×10 ⁹	12	26
20	$NO_3^{\bullet} + NO_3^{\bullet} \rightarrow N_2O_6$	3.0×107 L mol-1s-1	32	6.0×10 ⁷	2	d
21	$NO_3 + OH \rightarrow OH + NO_3$	8.2×107 L mol-1s-1	27	1.0×10 ¹⁰	12	d
22	$NO_3^{\bullet} + H_2O \rightarrow OH + HNO_3$	0.9 M ⁻¹ s ⁻¹	33	4.7×10 ²	16	d
23	$NO_3^{\bullet} + HO_2^{\bullet} \rightarrow NO_3^{-} + H^+ + O_2$	3.0×10 ⁹ L mol ⁻¹ s ⁻¹	28	4.5×10 ⁹	1	d
24	$\operatorname{NO}_3^{\bullet} + \operatorname{S}_2\operatorname{O}_8^{2^{\circ}} \longrightarrow \operatorname{NO}_3^{-} + \operatorname{S}_2\operatorname{O}_8^{\bullet}$	1.0×10 ⁴ L mol ⁻¹ s ⁻¹	24			
		1.0×10 ⁴ L mol ⁻¹ s ⁻¹	*	3.6×10 ⁷	27	*Table S16
25	$NO_3^{\bullet} \rightarrow products$	$47\pm19~s^{\text{-1}}$	*Table S17	-	-	-
26a	SO_4^{-} + PENTOL \rightarrow PENTOL alkyl	9.4×10 ⁸ L mol ⁻¹ s ⁻¹	*Table 1	7.9×10 ⁹	5	*Table 7
26b	SO_4^- + HEXOL \rightarrow HEXOL alkyl	2.5×10 ⁹ L mol ⁻¹ s ⁻¹	*Table 1	1.1×10 ¹¹	10	*Table 7
26c	SO_4^- + HEXAL \rightarrow HEXAL alkyl	4.8×10 ⁸ L mol ⁻¹ s ⁻¹	*Table 1	2.9×10 ⁹	5	*Table 7
27	GLV alkyl + $O_2 \rightarrow GLV$ peroxy	2.0×10 ⁹ L mol ⁻¹ s ⁻¹	34	8.5×10 ¹¹	15	35
28	$2 \text{ GLV peroxy} \rightarrow \text{GLV p}$	1.6×10 ⁸ L mol ⁻¹ s ⁻¹	36	5.9×10 ⁸	3	37
29	OH+ GLV peroxy→GLV p1	9.6×10 ¹⁰ L mol ⁻¹ s ⁻¹	b, 38	1.4×10 ¹¹	1	26
30	$NO_3^{+} GLV peroxy \rightarrow GLV p2$	1.2×10 ⁹ L mol ⁻¹ s ⁻¹	b, 39	1.8×10 ⁹	1	26
31	$SO_4^- + GLV \text{ peroxy} \rightarrow GLV \text{ p3}$	3.5×10 ⁹ L mol ⁻¹ s ⁻¹	a, 28	5.2×10 ⁹	1	26
32a	$NO_3^{\bullet} + PENTOL \rightarrow PENTOL alkyl2$	1.5×10 ⁸ L mol ⁻¹ s ⁻¹	*Table 3	1.5×10 ¹¹	17	*Table 7
32b	$NO_3^{\bullet} + HEXOL \rightarrow HEXOL alkyl2$	8.4×10 ⁸ L mol ⁻¹ s ⁻¹	*Table 3	3.8×10 ¹⁰	9	*Table 7
32c	$NO_3^{\bullet} + HEXAL \rightarrow HEXAL alkyl2$	3.0×107 L mol ⁻¹ s ⁻¹	*Table 3	3.2×10 ¹⁰	17	*Table 7
1			1			

^a adopted from the reaction of SO₄[•] with HO₂[•]; ^b adopted from gas-phase reactions of RO₂[•] radicals, *This work; ^c an average of the activation energy of reaction 7 and 8; ^d Ea from corresponding reactions of SO₄[•] radicals, and A values calculated using the rate constants at 298 K

Kinetic parameters for reactions (13), (15), (24), and (25) in Table S13

The kinetic parameters for reactions

$$SO_4^{\bullet} + NO_3^{\bullet} \rightarrow NO_3^{\bullet} + SO_4^{2-}$$
(13)

$$SO_4^{\cdot} + S_2O_8^{2-} \longrightarrow S_2O_8^{\cdot} + SO_4^{2-}$$

$$\tag{15}$$

$$NO_{3}^{\bullet} + S_{2}O_{8}^{2-} \longrightarrow NO_{3}^{-} + S_{2}O_{8}^{\bullet-}$$
(24)

$$NO_3^{\bullet} \rightarrow \text{products}$$
 (25)

were estimated in this work from the experimental data collected during the background blank runs which were done in the same way as regular $GLV + NO_3$ runs but without a GLV added. We analyzed the data with COPASI software using a built-in evolutionary algorithm (200 generations and population size 20) or a trial-and-error approach. The results are presented in Tables S14 – S17 along with the corresponding Arrhenius equations S23 – S25.

Table S14. The ter	SolutionSoluti							
	k (L mol ⁻¹ s ⁻¹)							
278 K	288 K	298 K	308 K	318 K				
4.5×10 ⁴	6.4×10 ⁴	9.0×10 ⁴	1.2×10 ⁵	1.7×10^{5}				
6.7×10 ⁴	8.4×10^{4}	9.1×10 ⁴	8.4×10^4	-				
5.4×10 ⁴	7.0×10^4	9.5×10 ⁴	1.5×10 ⁵	1.9×10 ⁵				
Average								
$(5.5 \pm 1.1) \times 10^4$	$(7.3 \pm 1.0) \times 10^4$	$(9.2 \pm 0.3) \times 10^4$	$(1.2 \pm 0.3) \times 10^5$	$(1.8 \pm 0.1) \times 10^5$				

$$k(T) = 4.1 \times 10^8 \exp\left(-\frac{2490 \pm 210}{T}\right) L \ mol^{-1} \ s^{-1}$$
(S23)

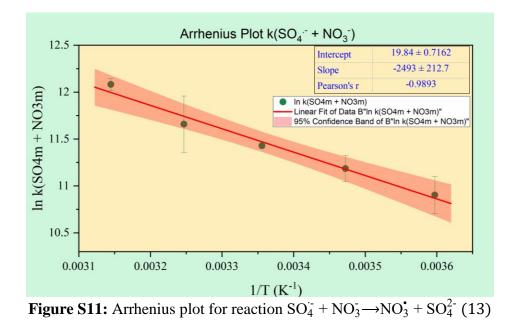


Table S15. The temperature-dependent rate constants for reaction (15).

$SO_4^{-} + S_2O_8^{2-} \longrightarrow S_2O_8^{-} + SO_4^{2-}$ (15)								
	k (L mol ⁻¹ s ⁻¹)							
278 K	288 K	298 K	308 K	318 K				
5.0×10 ⁴	8.0×10^4	2.2×10^4	1.0×10^{4}	6.0×10 ³				
5.0×10 ⁴	5.0×10 ⁴	1.0×10^{4}	1.0×10 ³	-				
7.6×10 ⁴	5.0×10 ⁴	1.0×10^{4}	1.0×10^{4}	2.0×10 ³				
Average								
$(5.9 \pm 1.5) \times 10^4$	$(6.0 \pm 1.7) \times 10^4$	$(1.4 \pm 0.7) \times 10^4$	$(7.0 \pm 5.2) \times 10^3$	$(4.0 \pm 2.8) \times 10^3$				
		Average						

$$k(T) = 2.2 \times 10^{6} \exp\left(-\frac{-7190 \pm 1230}{T}\right) L \ mol^{-1} \ s^{-1}$$
(S24)

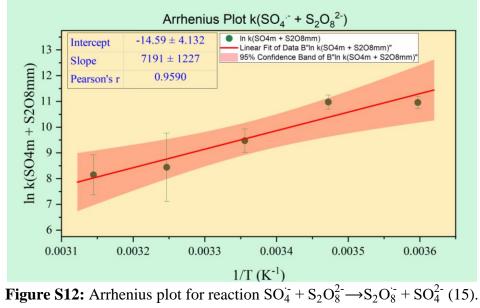
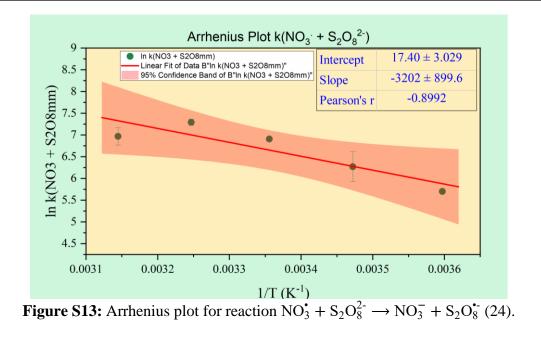


Table S16. The temperature-dependent rate constants for reaction (24).
$NO^{*} + SO^{2-} > NO^{-} + SO^{*-} (24)$

k (L mol ⁻¹ s ⁻¹)								
278 K 288 K 298 K 308 K 318 K								
2×10 ³	3×10 ³	1×10^{4}	1.6×10^{4}	4.0×10^{4}				
2×10 ³	4.4×10^{3}	1×10^{4}	1.8×10 ³	-				
2×10 ³	6×10 ³	1×10^{4}	1.6×10 ⁴	3.0×10 ⁴				
Average								
2×10 ³	$(4.5 \pm 2.5) \times 10^3$	1.0×10 ⁴	$(1.7 \pm 0.8) \times 10^4$	(3.5 ± 2.1)×10				

$$k(T) = 3.6 \times 10^7 \exp\left(-\frac{3200 \pm 900}{T}\right) L \, mol^{-1} \, s^{-1} \tag{S25}$$



The first-order decay of NO_3 radicals occurred in all experiments, but its rate did not depend on temperature. Probably, the sink can be explained through some physical processes like the wall loss of radicals. The magnitude of this sink was smaller than 10% of the total sink of NO_3 without the reaction with GLV. Therefore, we suggest using the average value across the temperature range we studied.

Table S17. The estimation of the rate constants for the first-order sink of NO3 radicals. $NO_3^{\bullet} \rightarrow products$							
Average k (s ⁻¹)							
278 K	288 K	298 K	308 K	318 K	278-318 K		
					average		
49	67	32	64	25	47 ± 19		

Estimation of the GLV + NO₃[•] rate constants at T = 278 K, 288 K, 298 K. 308 K, and 318 K

The temperature-dependent second-order rate constants for the reaction of GLV with NO₃[•] were estimated from the experimental data using Model_1 reactions and the COPASI parameter estimation task with the evolutionary programming method (number of generations 200, population size 20). The estimated values of rate constant k_{32} at individual temperatures are summarized in Tables S7-S9. The experimental and model traces are compared below in Figure S13-S25. According to the experimental conditions, the initial non-zero concentrations of reactants were: 0.03 mol L⁻¹ for S₂O₈²⁻ and 0.1 mol L⁻¹ for NO₃⁻. The initial SO₄⁺⁻ radical concentration was $(2.3 \pm 0.1) \times 10^{-7}$ mol L⁻¹ as calculated from the excimer laser's emitted energy in the experiments. The concentration of GLV was varied $(0 - 1 \times 10^{-4} \text{ mol L}^{-1}\text{s}^{-1})$ and is specified on the plots (Figure S13-S24).

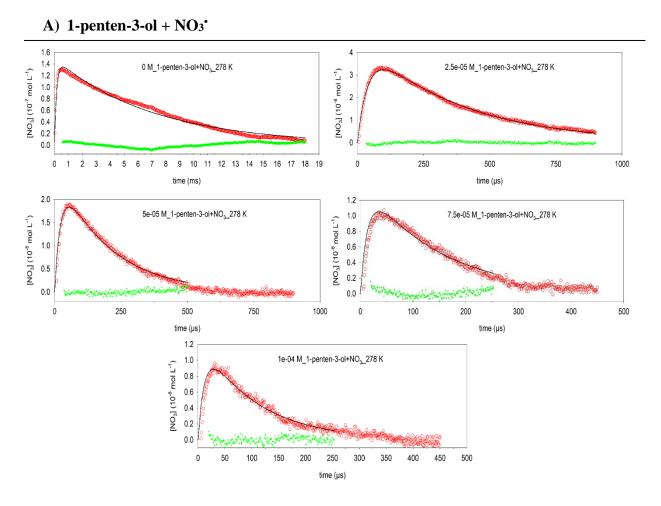


Figure S14. Concentration-time-profiles of NO₃[•] in experiments at 278 K and various initial concentrations of 1-penten-3-ol (specified in the legends). Experimental data points are shown as red circles, simulation - as black lines, and residuals - as green crosses.

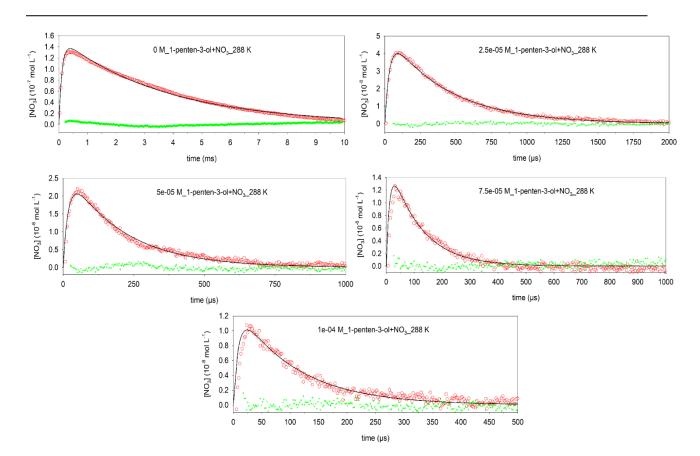


Figure S15. Concentration-time-profiles of NO₃[•] in experiments at 288 K and various initial concentrations of 1-penten-3-ol (specified in the legends). Experimental data points are shown as red circles, simulation - as black lines, and residuals - as green crosses.

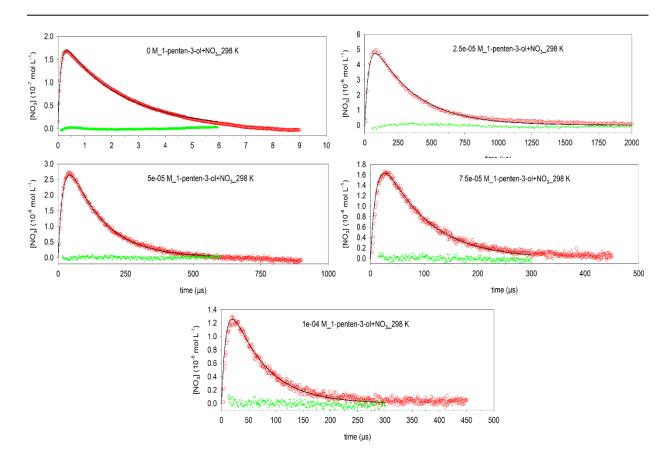


Figure S16. Concentration-time-profiles of NO₃[•] in experiments at 298 K and various initial concentrations of 1-penten-3-ol (specified in the legends). Experimental data points are shown as red circles, simulation - as black lines, and residuals - as green crosses.

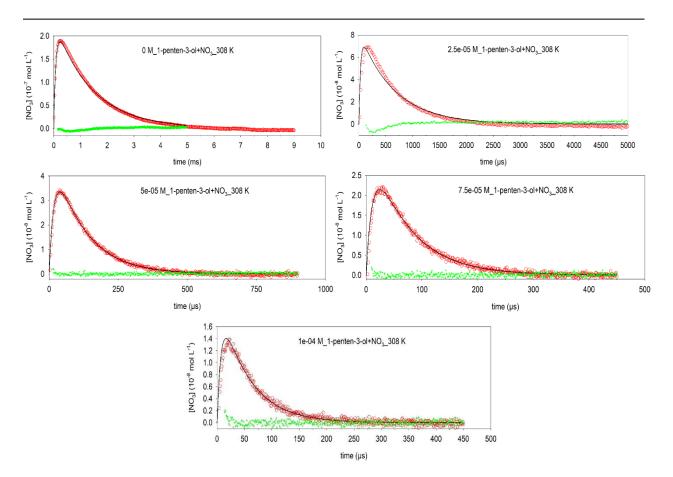


Figure S17. Concentration-time-profiles of NO₃[•] in experiments at 308 K and various initial concentrations of 1-penten-3-ol (specified in the legends). Experimental data points are shown as red circles, simulation - as black lines, and residuals - as green crosses.

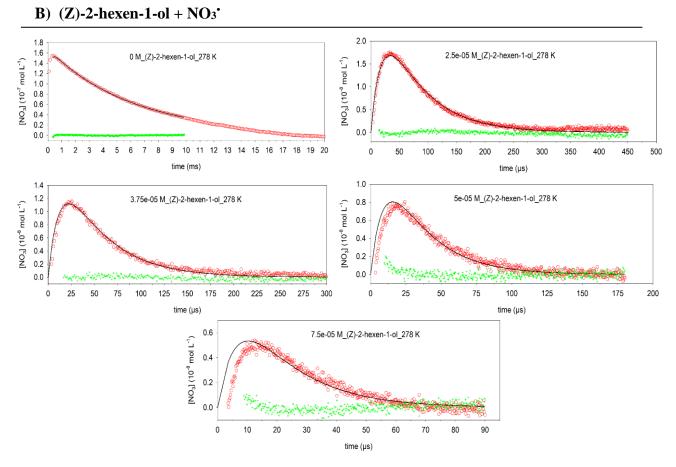


Figure S18. Concentration-time-profiles of NO₃[•] in experiments at 278 K and various initial concentrations of (Z)-2-hexen-1-ol (specified in the legends). Experimental data points are shown as red circles, simulation - as black lines, and residuals - as green crosses.

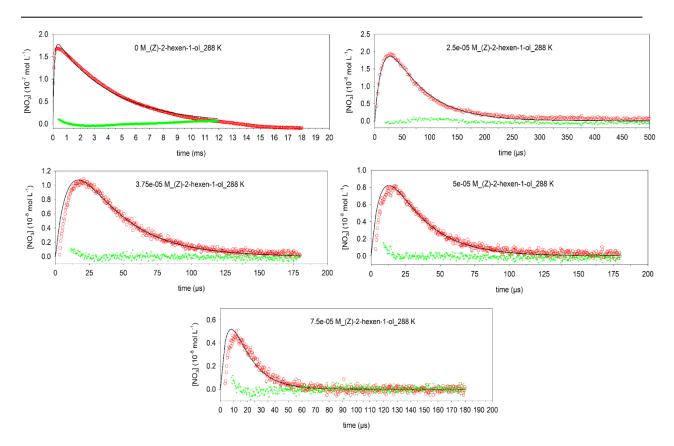


Figure S19. Concentration-time-profiles of NO₃ in experiments at 288 K and various initial concentrations of (Z)-2-hexen-1-ol (specified in the legends). Experimental data points are shown as red circles, simulation - as black lines, and residuals - as green crosses.

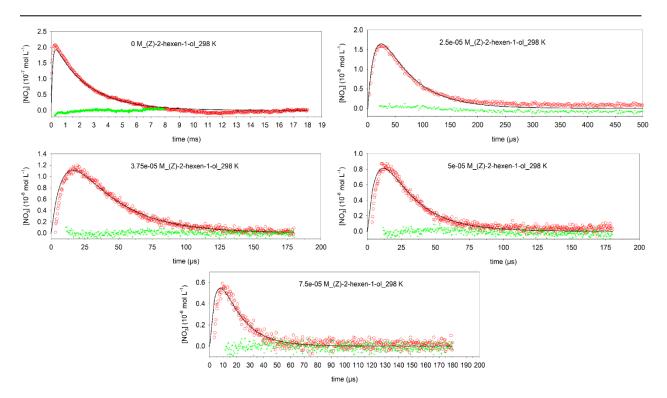


Figure S20. Concentration-time-profiles of NO₃[•] in experiments at 298 K and various initial concentrations of (Z)-2-hexen-1-ol (specified in the legends). Experimental data points are shown as red circles, simulation - as black lines, and residuals - as green crosses.

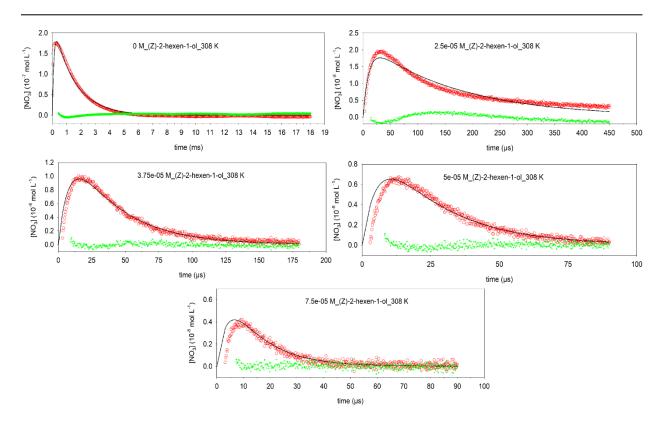


Figure S21. Concentration-time-profiles of NO₃[•] in experiments at 308 K and various initial concentrations of (Z)-2-hexen-1-ol (specified in the legends). Experimental data points are shown as red circles, simulation - as black lines, and residuals - as green crosses.

C) (E)-2-hexen-1-al + NO₃·

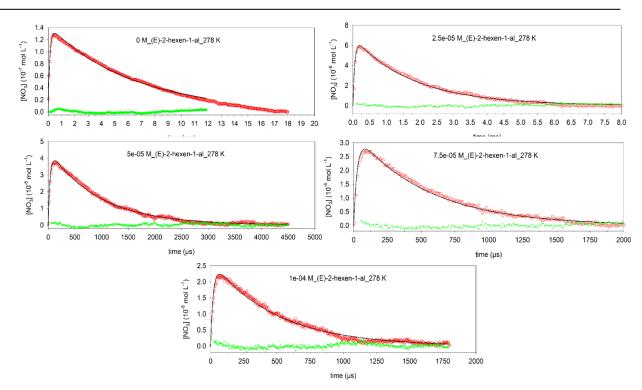


Figure S22. Concentration-time-profiles of NO₃[•] in experiments at 278 K and various initial concentrations of (E)-2-hexen-1-al (specified in the legends). Experimental data points are shown as red circles, simulation - as black lines, and residuals - as green crosses.

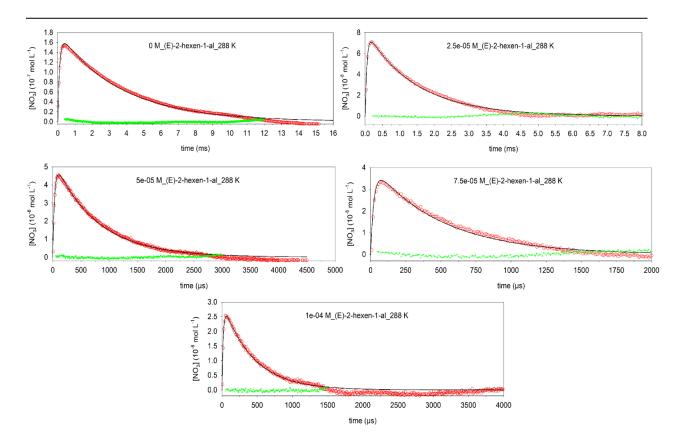


Figure S23. Concentration-time-profiles of NO₃[•] in experiments at 288 K and various initial concentrations of (E)-2-hexen-1-al (specified in the legends). Experimental data points are shown as red circles, simulation - as black lines, and residuals - as green crosses.

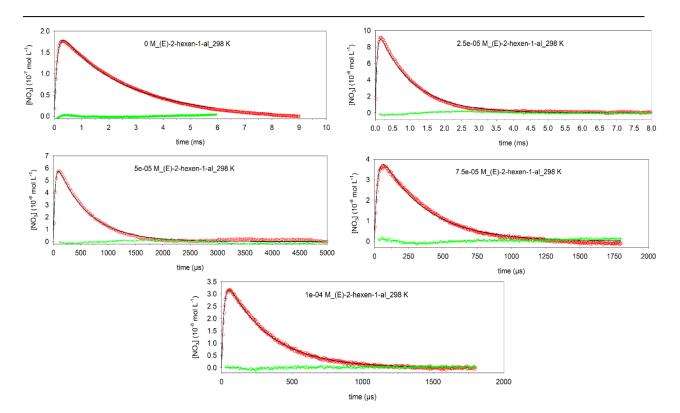


Figure S24. Concentration-time-profiles of NO₃[•] in experiments at 298 K and various initial concentrations of (E)-2-hexen-1-al (specified in the legends). Experimental data points are shown as red circles, simulation - as black lines, and the residuals - as green crosses.

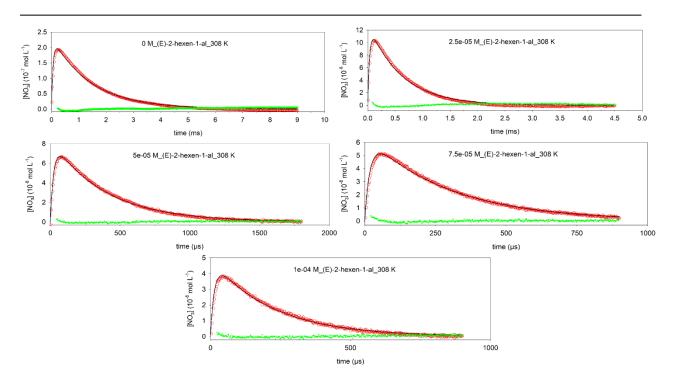


Figure S25. Concentration-time-profiles of NO₃ in experiments at 308 K and various initial concentrations of (E)-2-hexen-1-al (specified in the legends). Experimental data points are shown as red circles, simulation - as black lines, and residuals - as green crosses.

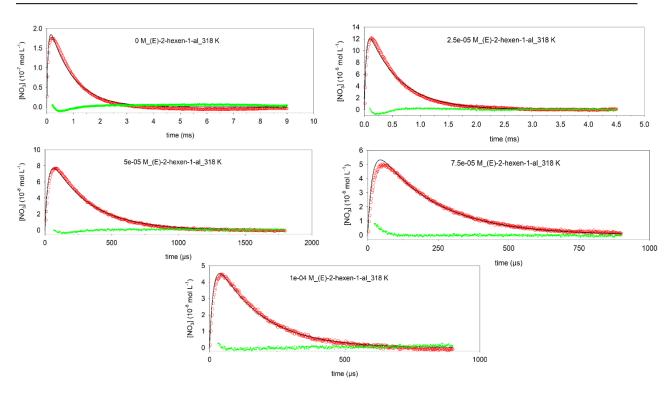


Figure S26. Concentration-time-profiles of NO₃[•] in experiments at 318 K and various initial concentrations of (E)-2-hexen-1-al (specified in the legends). Experimental data points are shown as red circles, simulation - as black lines, and residuals - as green crosses.

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